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Roll:.....*1800130*.....

# Fluid Mechanics

## # Course Content:

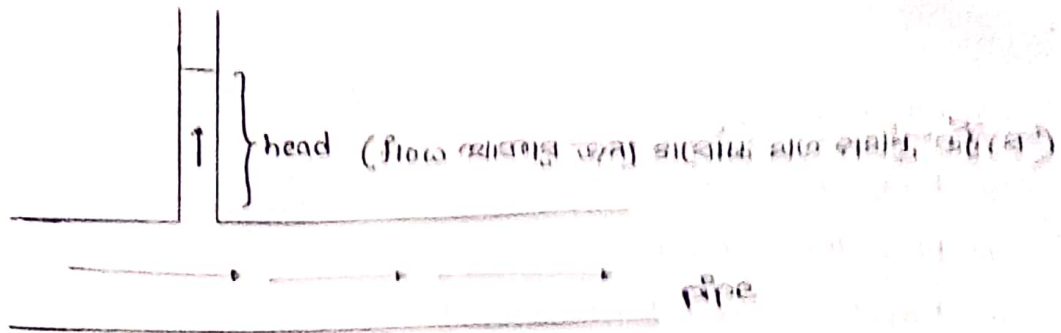
- ① Fluid dynamics
- ② Fluid measurement
- ③ Flow through pipes
- ④ Laminar and turbulent flow
- ⑤ Study in compressive flow in pressure conduites.
- ⑥ Similitude and dimensional analysis.

## # Why fluid dynamic is essential for us:

- ① Fluid dynamics is changing our world.
- ② " " is the study of fluid in motion or fluid flow.
- ③ " " affects every aspects of our life.
- ④ " " helps us to understand how our world works.
- ⑤ " " affects the blood flow to our brain and heart.

# Types of head of fluid in motion:

↳ rise of water



3 types:

① Potential head or potential energy: This is due to configuration or position above some suitable datum lines.

It is denoted by  $z$ . (also known as datum head)

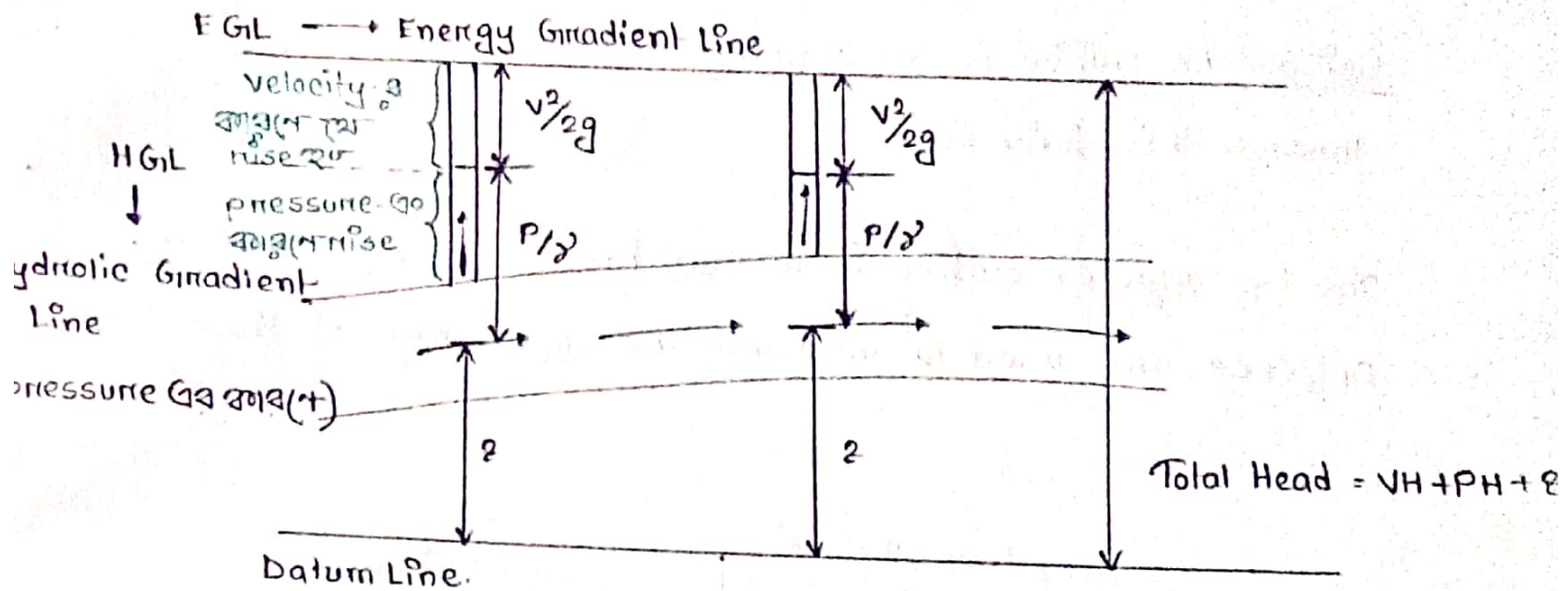
② Velocity head or kinetic energy: This is due to velocity of flowing liquid and is measured as  $\frac{v^2}{2g}$ .

③ Pressure head or pressure energy: This is due to the pressure of liquid and is measured as  $\frac{P}{\rho g}$ .

$$* z = \frac{P}{\rho g}$$

\* total head = total energy per unit weight

(pressure, velocity, gravity potential / নিচে এর কারণ (যে point পাওয়া যায়))



Bernoulli's eqn: Total head of energy cons.

channel এর তেঁত্রে প্রত্যেক fluid এর property same

In an ideal incompressible fluid when the flow is steady and continuous, sum of pressure energy, kinetic energy and potential energy is constant along a stream / fluid line.

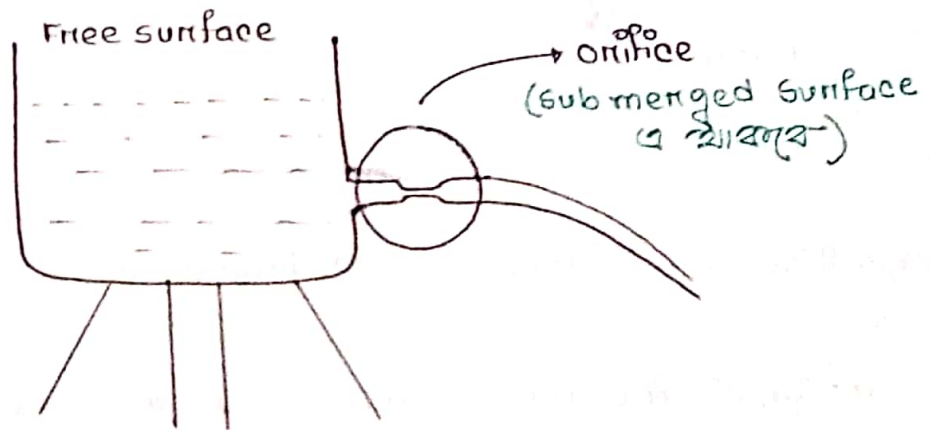
Mathematically:  $P/\rho + \frac{v^2}{2g} + z = \text{constant}$

## # Flow through orifice and mouthpiece:

Orifice: An orifice is an opening in the wall or base of a vessel through which fluid flows.

The top edge of orifice is always below the free surface.

Orifices are used to measure the discharge of fluid flow.



## # Classification of orifice:

① According to size:

- ① Small orifice
- ② Large orifice

② According to the shape of orifice:

- ① circular orifice
- ② Rectangular "
- ③ Square "
- ④ Triangular "

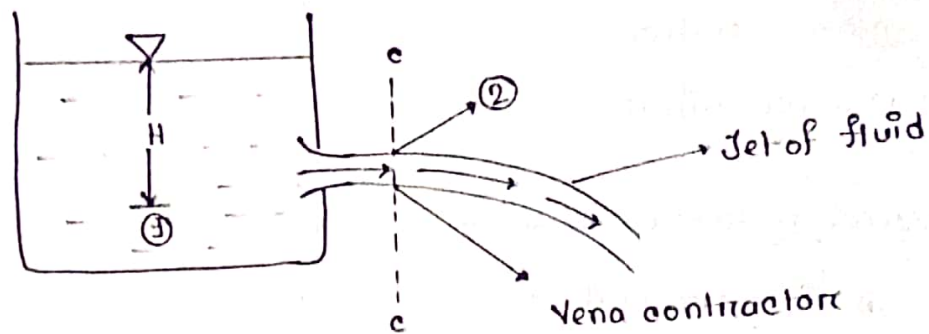
③ According to the shape of upstream edge:

- ① sharp edged orifice
- ② Bell-mouthed orifice

④ According to discharge condition:

- ① Free discharge orifice
- ② Submerged "
- ③ Partially submerged "
- ④ Fully submerged "

## # Torricelli's Theorem:



Consider 2 points ① and ② as shown in figure. Point ① is at the  
-the and point ② is the venacontractor.

↓  
It is a point where cross sectional area  
minimum and velocity maximum.

(when the water is normally flowing)

Let, the flow is steady and at a constant head  $H$ , applying  
Bernoulli's eqn at point ① and ② gives,

$$\frac{P_1}{\rho g} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{v_2^2}{2g} + z_2$$

point- ① and ② same level,  $\therefore z_1 = z_2$

$$\therefore \frac{P_1}{\rho g} + \frac{v_1^2}{2g} = \frac{P_2}{\rho g} + \frac{v_2^2}{2g}$$



We can write,

$$\frac{P_1}{\rho g} = H$$

$$\begin{cases} P = \rho H \\ \therefore P \propto H \end{cases}$$

For point ②  $\rightarrow$

$$\frac{P_2}{\rho g} = 0 \quad [\text{atmospheric pressure}]$$

For ① velocity  $v_1$ , for ② velocity  $v_2 \rightarrow \therefore v_2 \gg v_1$

$\therefore v_1 = 0$  [ $v_1$  is very small in comparison to  $v_2$  as area of tank is very large as compared to area of jet of the fluid.]

From ③  $\rightarrow$

$$H + 0 = 0 + \frac{v_2^2}{2g}$$

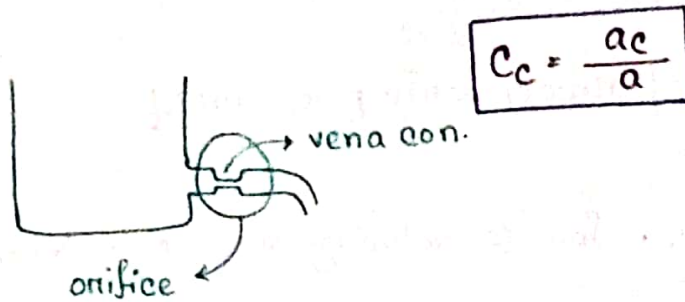
$$\Rightarrow \boxed{v_2 = \sqrt{2gH}}$$

This is theoretical velocity.

Actual velocity will be less than this value.

# Hydraulic co-efficiency:  $(C_d, C_c, C_v, C_r) \rightarrow 4 \text{ types}$

$C_c \rightarrow$  Co-efficient of contraction =  $\frac{\text{Area of jet of Vena Contracta}}{\text{Area of orifice}}$



$C_r \rightarrow$  Co-efficient of resistance is the ratio of loss of head in the orifice to the head of water available at the exit of the orifice is known as co-efficient of resistance.

It is denoted by  $C_r$ .

$$C_r = \frac{\text{loss of head of orifice}}{\text{Head of water}}$$

$C_d \rightarrow$  Co-efficient of discharge

$$C_d = \frac{\text{Actual discharge}}{\text{Theoretical discharge}} = \frac{Q}{Q_{th}} = C_d$$

$$= \frac{\text{Actual velocity} \times \text{Actual area}}{\text{Theoretical velocity} \times \text{Theoretical area}}$$

(Finved)

# Standard value for hydraulic co-efficiencies:

- (i) Co-efficient of velocity,  $C_v = 0.95 - 0.99$
- (ii) " " contraction,  $C_c = 0.61 - 0.69$
- (iii) " " discharge,  $C_d = 0.61 - 0.65$

Prob: An orifice is 50 mm in diameter. It is discharging water under a head of 9 meters. If  $C_d = 0.6$  and  $C_v = 0.9$ . Find actual discharge, actual velocity of jet at vena contracta.

→  $d = 50 \text{ mm}$   
 $H = 9 \text{ m}$   
 $C_v = 0.9$   
 $C_d = 0.6$

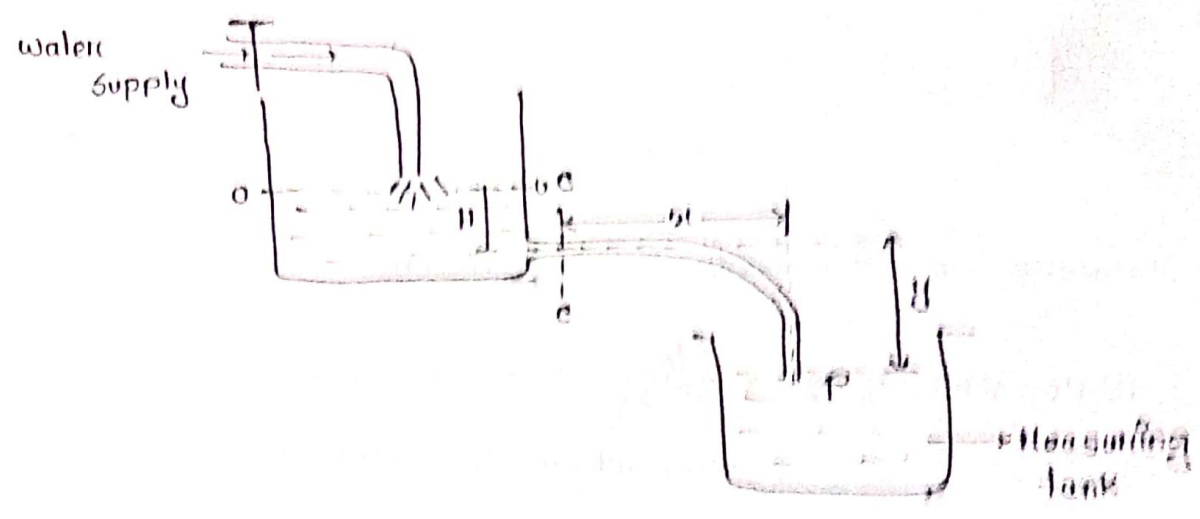
$$C_d = \frac{\text{Actual discharge}}{\text{Theoretical discharge}}$$

$$\Rightarrow Q_{in} = a \times \sqrt{2gH}$$

$$a = \frac{1}{4} \pi d^2 \rightarrow \text{area of orifice}$$

$$C_v = \frac{\text{Actual velocity}}{\text{Theoretical velocity}}$$

# Determination of Hydraulic coefficient by orifice method



① Determination of coefficient of velocity:

Figure shows a tank containing water at a constant level, maintained by a constant supply. Let the water flow out of the tank through a orifice fitted in one side of the tank.

Let the section c-c represents the point of vena contraction

Consider a particle of water in the jet at p.

Let,  $x$  = horizontal distance travelled by the particle at time  $t$ .

$y$  = Vertical distance bet<sup>n</sup> c-c and p.

$v_c$  = Actual velocity of the jet at vena contraction.

$H = \text{constant water head.}$

$\therefore \text{Horizontal distance, } x = vt \quad \text{--- (i)}$

$\text{Vertical distance, } y = \frac{1}{2}gt^2 \quad \text{--- (ii)}$

From eqn (i)  $\rightarrow$

$$t = \frac{x}{v}$$

From (ii)  $\rightarrow$

$$y = \frac{1}{2}g \times \frac{x^2}{v^2} = \frac{gx^2}{2v^2}$$

$$\therefore v = \sqrt{\frac{gx^2}{2y}}$$

Actual velocity.

$$\therefore C_v = \frac{\text{Act. velocity}}{\text{Theor. velocity}}$$

$$= \frac{\sqrt{\frac{gx^2}{2y}}}{\sqrt{2gH}}$$

$$C_v = \frac{x}{\sqrt{4yH}}$$

# Determination of co-efficient of discharge:

The water flowing through the orifice under the cons. head  $H$  is collected in a measuring tank for a known time  $t$ .

The rise of water level in the measuring tank is noted down.

The actual discharge through the orifice.

$$Q = \frac{\text{Area of measuring tank} \times \text{rise of water level in the measuring tank}}{\text{time } (t)}$$

$$\text{Theoretical discharge, } Q_{th} = \text{Area of orifice} \times \sqrt{2gH}$$

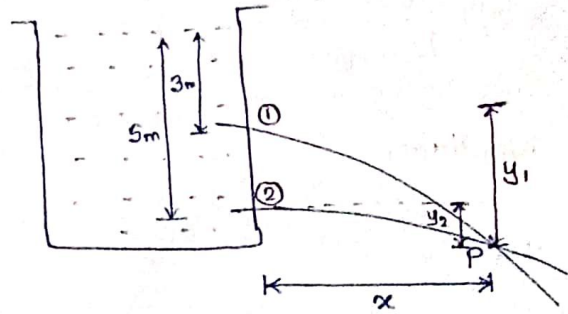
$$= a \times V_{th}$$

$$= a \times \sqrt{2gH}$$

$$C_d = \frac{Q}{Q_{th}}$$

$$C_d = \frac{Q}{a \times \sqrt{2gH}}$$

# Prob: A tank has two identical orifices on one of its vertical side. The upper orifice is 3 meter below the water surface and lower one is 5m below the water surface. If the value of  $C_v$  for each orifice 0.96. Find the point of intersections of 2 jets.



⇒ Height of water from orifice, 1,  $H_1 = 3m$   
 $H_2 = 5m$

Let  $P$  is the point of intersection of 2 jets coming from orifice 1 and 2.

$x$  = hor. dis from  $P$ .

$y_1$  = ver. dis from orifice ①

$y_2$  = ver. dis from orifice ②

$$y_1 = y_2 + (5-3)$$

$$\Rightarrow y_1 = y_2 + 2$$

For orifice ①  $\longrightarrow$

$$C_{v_1} = \frac{\alpha}{\sqrt{4y_1 H_1}} \quad [H_1 = 3 \text{ m}]$$

$\longleftarrow$  ①

For orifice ②  $\longrightarrow$

$$C_{v_2} = \frac{\alpha}{\sqrt{4y_2 H_2}} \quad [H_2 = 5 \text{ m}]$$

$\longleftarrow$  ②

① and ② are identical,

$$C_{v_1} = C_{v_2}$$

$$\Rightarrow \frac{\alpha}{\sqrt{4y_1 H_1}} = \frac{\alpha}{\sqrt{4y_2 H_2}}$$

$$\Rightarrow \frac{\alpha}{\sqrt{12(y_2 + 2)}} = \frac{\alpha}{\sqrt{20y_2}}$$

$$\Rightarrow y_2 = 3 \text{ m}$$

$y_2$  এর মান ① নং এ বসিয়ে,

$$0.96 = C_{v_1} = \frac{\alpha}{\sqrt{4 \times 5 \times 3}}$$

$$\Rightarrow \alpha = 7.24 \text{ m}$$

\*  
Ex. 8.8

### # Flow through large orifice:

① Available head of a liquid is less than 5 times the height of orifice.  
point A point B velocity change  $v_1 \rightarrow$  discharge change  $v_2$ .

$$Q = C_d \times (b \times d) \times \sqrt{2gH}$$

$\downarrow$   
 $H_2 - H_1$

Discharge through a large orifice:

large:  $Q = \frac{2}{3} C_d \times b \sqrt{2g} [H_2^{3/2} - H_1^{3/2}]$

small:  $Q = C_d \times a \times \sqrt{2gH}$   $\rightarrow H_1 = d/2$

# Mouth piece: extension of pipe  
 $\rightarrow$  length 2 to 3 time dia.

Classification of mouthpiece.

Flow through an external cylindrical mouthpiece.

eddy loss head loss  $h_l = \frac{(v_1 - v_2)^2}{2g}$

actual,  $v = 0.855 \sqrt{2gH}$

$$C_d = C_v \times C_c$$

theoretical,  $v_t = \sqrt{2gH}$

\*  
# কোন mouthpiece ও orifice এর ক্ষেত্রে discharge (কিভাবে হয়?)

# Practice Prob: 13

# Time required for emptying a hemispherical tank.

$$T = \frac{\pi}{C_d \sqrt{2g}}$$

# Bansal prob - 7-19 (page 334)

Flow over notches and weirs:

V-notch  
masonry

notch and weir:

↳ submerged condition & থাকবে

Nappe and crest:

Types of Notches:

(i) Steeped notch.

(ii)  
(iii)  
(iv)

Types of weir:

# Discharge over a Rectangular Notch or weir:

$$\text{Area of strip} = A = L \times dh$$

$$dQ = C_d L dh \sqrt{2gh}$$

$$Q = \frac{2}{3} C_d L \sqrt{2g} [H]^{3/2}$$

Practic prob #14

# Discharge over a triangular Notch or Weir:

$$\text{Area of strip} = 2 \tan \theta/2 \times (H-h) \times dh$$

$$Q = 2 C_d \tan \theta/2 \times \sqrt{2g} \left[ \frac{Hh^{3/2}}{3/2} - \frac{h^{5/2}}{5/2} \right]_0^H$$

$$= \frac{8}{15} C_d \tan \theta/2 \times \sqrt{2g} \times H^{5/2}$$

Practice Prob# 15

$$Q = \frac{2}{3} C_d L \sqrt{2g} H^{3/2}$$

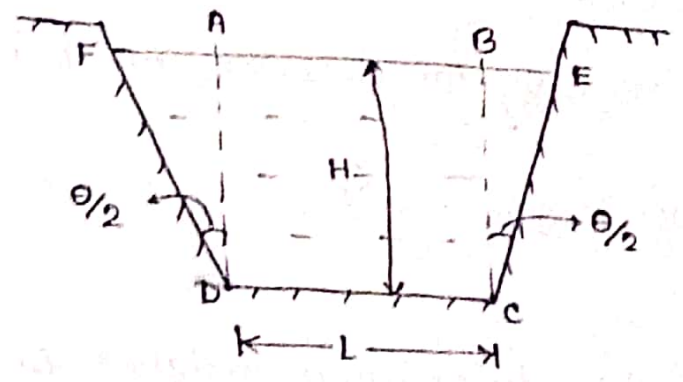
$$Q = \frac{8}{15} C_d \tan \frac{\theta}{2} \sqrt{2g} H^{5/2}$$

Ans: 357.2 mm

# Advantages of triangular notch over a rectangular weir:

- i) For a right-angle V-notch on weir, the expression for the computation of discharge is very simple. ( $Q = 1.417 H^{3/2}$ )
- ii) In a given triangular notch, only one reading that is Head (H) is required to be taken for the measurement of discharge.
- iii) For a low discharge, a triangular notch, keeps gives more accurate result than a rectangular notch.

Discharge over a trapezoidal notch on weir:



A trapezoidal notch on weir is a combination of a rectangular and triangular notch on weir. Thus total discharge will be equal to the sum of discharge through rectangular weir + discharge through triangular weir.



∴ Discharge through trapezoidal notch or weir

$$Q = Q_1 + Q_2$$

$$= \frac{2}{3} \times C_{d1} \times L \times \sqrt{2g} \times H^{3/2} + \frac{8}{15} \times C_{d2} \times \tan \frac{\theta}{2} \times \sqrt{2g} \times H^{5/2}$$

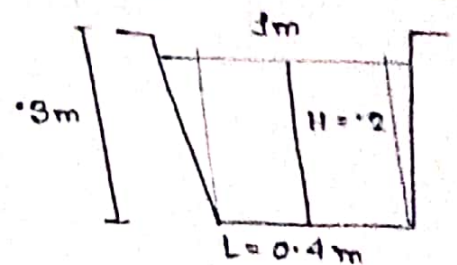
# Prob:

Find the discharge through a trapezoidal notch which is 3m wide at the top, 0.4 m at the bottom and 30 cm is in height. The head of water on the notch is 20 cm. Assume  $C_d$  for rectangular portion is 0.62, while triangular portion is equal to 0.6.

⇒

$$Q = \frac{2}{3} \times 0.62 \times \sqrt{2g} \times 0.4 \times 0.2^{3/2} + \frac{8}{15} \times 0.6 \times 1 \times \sqrt{2g} \times 0.2^{5/2}$$

$$= 0.091$$



$$\tan \frac{\theta}{2} = \frac{0.3}{0.3} = 1$$

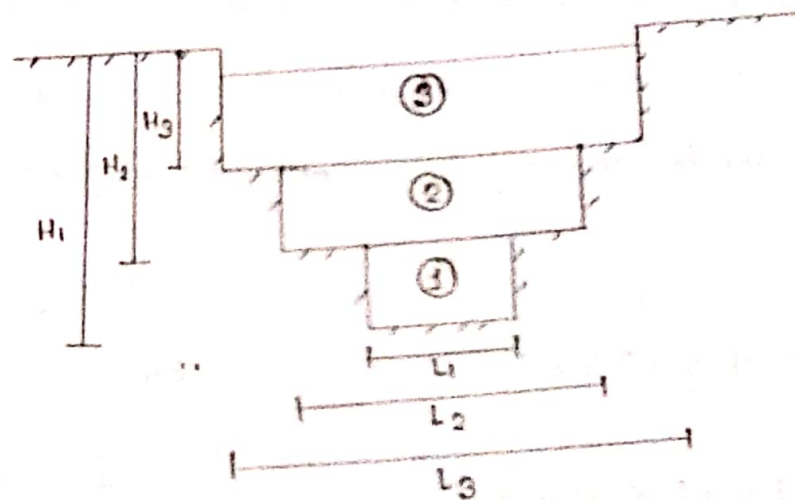
\* Step notch or weir: Trapezoidal weir.

- Discharge over stepped notch.

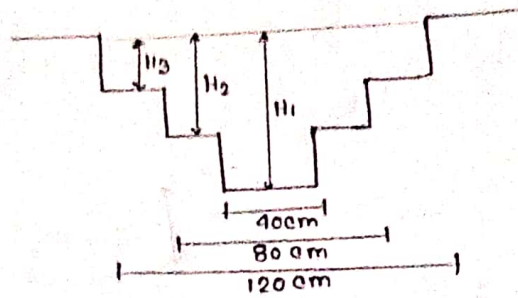
A stepped notch is a combination of rectangular notches.

The discharge through stepped notch is equal to the sum of discharges through different rectangular notches.

Consider a stepped notch as shown in Fig 8.6.



# Practice Problem #17



Sol<sup>n</sup>:

$$C_d = 0.62$$

$$L_1 = 40 \text{ cm}$$

$$L_2 = 80 \text{ cm}$$

$$L_3 = 120 \text{ cm}$$

$$H_1 = 50 + 30 + 15 = 95 \text{ cm}$$

$$H_2 = 50 + 30 = 80 \text{ cm}$$

$$H_3 = 50 \text{ cm}$$

$$Q_1 = \frac{2}{3} C_d \times L_1 \times \sqrt{2g} [H_1^{3/2} - H_2^{3/2}]$$

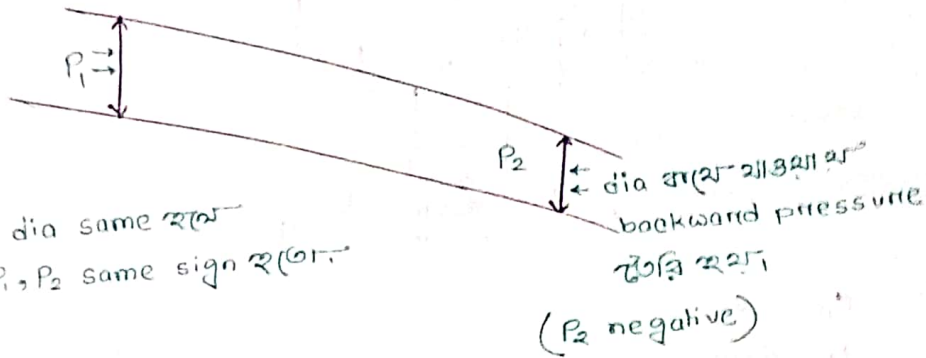
\* Cipolletti weir or notch

\* Broad crested weir, narrow crested weir.

✓\* Ogee weir, ogee notch. → definition + figure.

# Lecture : 1 and 2

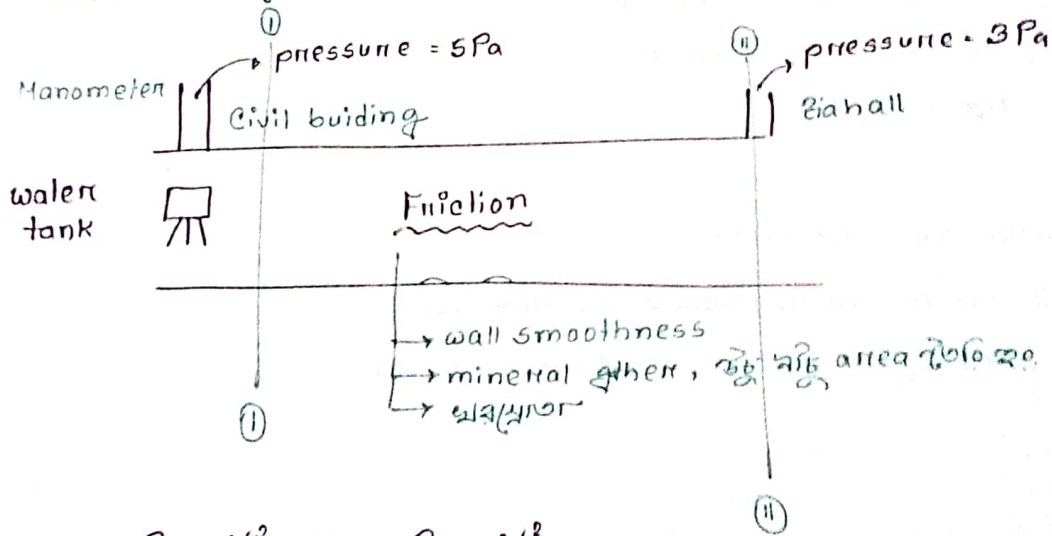
Derivation of- Bernoulli's eqn



Assumption

Bernoulli's eqn for real fluid:

Assignment → 6.4



$$\frac{P_1}{\rho} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2g} + z_2 + hf$$

$\rho = 59 \times \text{পারসর ঘনত্ব}$

Practical application of B.E.

Venturimeter.   
 → convergent   
 → divergent   
 → throat

Expression for rate of flow through venturimeter

$$\text{head loss } h = \frac{P_1 - P_2}{\rho g}$$

$$Q_{th} = \frac{a_1 a_2}{\sqrt{a_1^2 - a_2^2}} \times \sqrt{2gh}$$

Prac Prob # 4

# Lecture : 4 and 5# Pitot Tube:

velocity measurement.

Working of pitot tube:

Theory of pitot tube:

Q: → Arrangements of pitot tube: → 4.6 figure

Assignment: → 6.27, 6.45, Rajput (page-311), Prob-6, Prob-7, (Raj)-37  
Prob-8# Free liquid jet: → আঙ্গুল বাগানে (nozzle use করে) পানি  
প্রসারিত হয়

Trajectory path \*\*

Eqn of a free liquid jet.

Maximum Height attained by jet: